

HAYNES

An Investigation of the
Water Pressure Ejector

Civil Engineering

B. S.

1908

UNIVERSITY OF ILLINOIS
LIBRARY

Class

1908

Book

H33

Volume

My 08-15M



UNIVERSITY OF ILLINOIS
COLLEGE OF ENGINEERING
**AN INVESTIGATION OF THE
WATER PRESSURE EJECTOR**

BY
MARK ROSS HAYNES

THESIS
FOR THE
DEGREE OF BACHELOR OF SCIENCE
IN
CIVIL ENGINEERING

COLLEGE OF ENGINEERING

UNIVERSITY OF ILLINOIS

PRESENTED, JUNE, 1908

UNIVERSITY OF ILLINOIS

June 1, 1908

THIS IS TO CERTIFY THAT THE THESIS PREPARED UNDER MY SUPERVISION BY

MARK ROSS HAYNES

ENTITLED AN INVESTIGATION OF THE WATER PRESSURE EJECTOR

IS APPROVED BY ME AS FULFILLING THIS PART OF THE REQUIREMENTS FOR THE

DEGREE OF Bachelor of Science in Civil Engineering

Antalor

T. R. Agg.

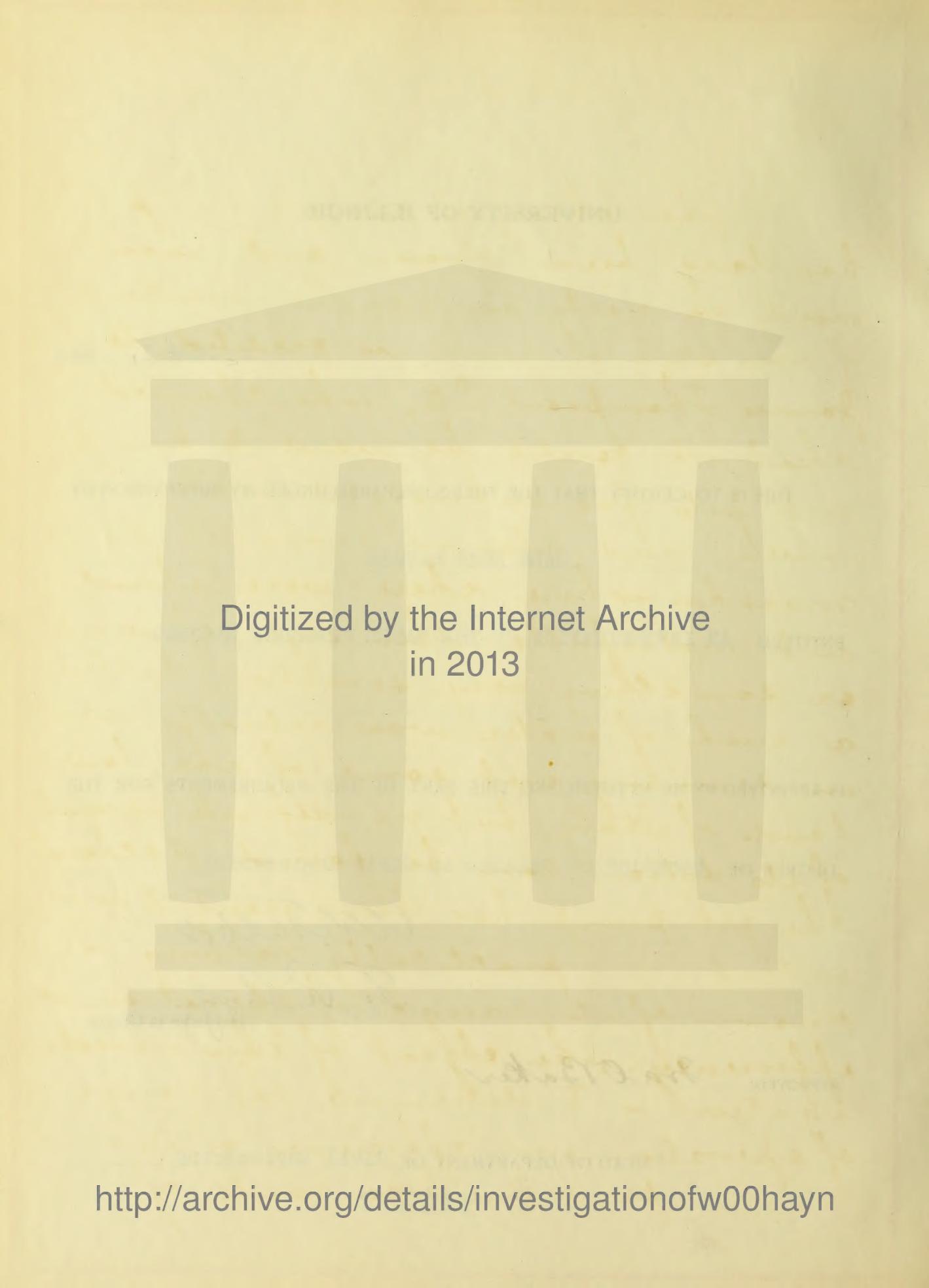
Instructor in Charge.

APPROVED:

Ira O. Baker

HEAD OF DEPARTMENT OF Civil Engineering

114582



Digitized by the Internet Archive
in 2013

<http://archive.org/details/investigationofw00hayn>

Theory

The theory of the jet pump has long been known and was used as early as 1850. The invention of this style of pump is credited to James Thompson C.E., who claimed that it could be used to pump out pits for submerged water wheels, and also in draining out marshes where there were abundant waterfalls. This style of pump or something very similar, called a rush of water was actually used in draining out some of the lowlands of Italy, but no definite account of its action can be found. Although the jet pump has been used to some extent, yet practically nothing is known of its range of operation or efficiency. The object of this investigation is to determine the range of operation and efficiency of two jet pumps. (1) One was made of



standard pipe fittings and constructed in the laboratory. (2) The other was an ordinary Chicago ejector and a slight modification of it.

These investigations were suggested by the idea that perhaps the jet pump could be used with satisfaction where there was plenty of water to be had at a fairly high pressure, a high efficiency not being necessary. These conditions would be found in the cities which owned their own water system and did their own sewer work.

Description of Apparatus

The apparatus was set up as shown in Plate I. The horizontal pipe A contains the water which is under pressure, this pressure being measured by the water gauge E. B is the suction pipe the bottom end of which is

always below the level of the water in the pit. D is a double elbow in the pipe so that the distance H may be made greater or smaller by inclining at a greater or less angle the discharge end C. The tank used to weigh the water is shown on the scales. These scales are standardized to be used in the department, so that their weights may be accepted as correct. G is the feeder pipe which supplies water to the pit as fast as it is pumped out through the suction pipe B. The hook gauge shown was used to make it easier to keep the level of the water at the same position during the run, and especially at the beginning and the end. The water meter at F was used to measure the quantity of water flowing through the feeder pipe during the run, this quantity also being equal to the amount pumped. This meter was calibrated before the experiments were started and

4

the calibration constants and tables are given in Table I. The valve K was used to regulate the flow in the feeder pipe so that the water could be allowed to flow in as fast as it was pumped out. The pit shown was about $6 \times 14 \times 5\frac{1}{2}$ feet deep. This depth limited the range of suction to five feet.

method of Testing.

The water in the pit was first brought to the desired level and the hook gauge was then raised or lowered until it just lifted the skin of the water in which position it was then clamped. The distance S or the suction distance was then measured and recorded. The inclined pipe C was placed at a certain angle and the distance H was measured and recorded. A reading was taken of the weight of the tank as indicated by the

scale and also a reading of the water meter and the run was ready to start.

At an initial time the valve at A was opened until the gauge E gave a certain head pressure which was recorded. The valve K in the feeder pipe G was now opened enough to keep the water level in the pit as constant as possible. A small variation of the level of the water in the pit did not make an appreciable difference in the results, providing that the levels at the beginning and end of the run were the same. The method employed was to keep the level of the water a fraction lower than the level at the start of the run, as this made it possible to stop the run at any time without the chance of having too much water in the pit. If on the other hand there was not enough water in the pit when the final readings were taken the

6.

water was allowed to run in the pipe G until the level was at the correct height. The experiment was allowed to run 8 or 10 minutes in which time the tank which holds about 32 cubic feet net capacity was about full, and then the shut-off valve A was closed and the time recorded. If the water in the pit was at the correct level as shown by the float gauge, the valve K was also closed. If this was not the case the valve K was left open until the float gauge showed the water to be at the correct level. Final readings were now taken of the water meter F, and the weight of the tank, and the experiment was finished.

Observations.

In order to obtain the efficiencies of all combinations of suction heads (S), pressure heads

(E) and lift heads H, the following method was employed. The suction head S was made as great as possible. The maximum value of S was about 5 feet as this was the difference which could be made in the levels of the water in the pit. The distance H was made as small as possible. The range of the distance H was from about 2 feet to 6 feet, that is, the end of pipe C could be raised or lowered through this distance without either striking the ceiling in one direction or the tank in the other.

Three reading were now taken using three different pressure heads. One as high as could be obtained, one at about the minimum that water could be pumped and the other midway between. The pressure heads used ranged from twenty to ninety feet. The next three readings were obtained in

8.

this manner. The suction head S was still kept the same but the distance H was increased about a foot. The three readings were taken by using the three different pressure heads as before. This method was kept up until the distance H was made as great as possible. The readings obtained so far will be called a set. In order to obtain Set II the suction distance S was decreased about two feet and the second set was taken as above described. In this manner all possible combinations that could be made were obtained.

Methods of calculating result and formulae used.

(1) Quantity pumped.

The quantity of water pumped was found in cubic feet per second by subtracting the final and initial

9

readings of the meter I , and dividing the result by the duration of time in seconds.

(2) Quantity used.

The total quantity flowing through the pipe C in pounds was found by subtracting the initial from the final reading of the scales. This was reduced to cubic feet per second by dividing the difference by 62.5 times the duration of run in seconds. The quantity used in cubic feet per second would be the number just found minus the number found under the quantity pumped.

Efficiency

Let W weight of water pumped

" W_2 = " " " used

" S = Value of suction head in feet

" H = distance as shown in figure

" D = Pressure head as given by gauge

" I = Efficiency

$$I = \frac{W, (S + H) + W_2 H}{(W, + W_2) D}$$

PLATE 1

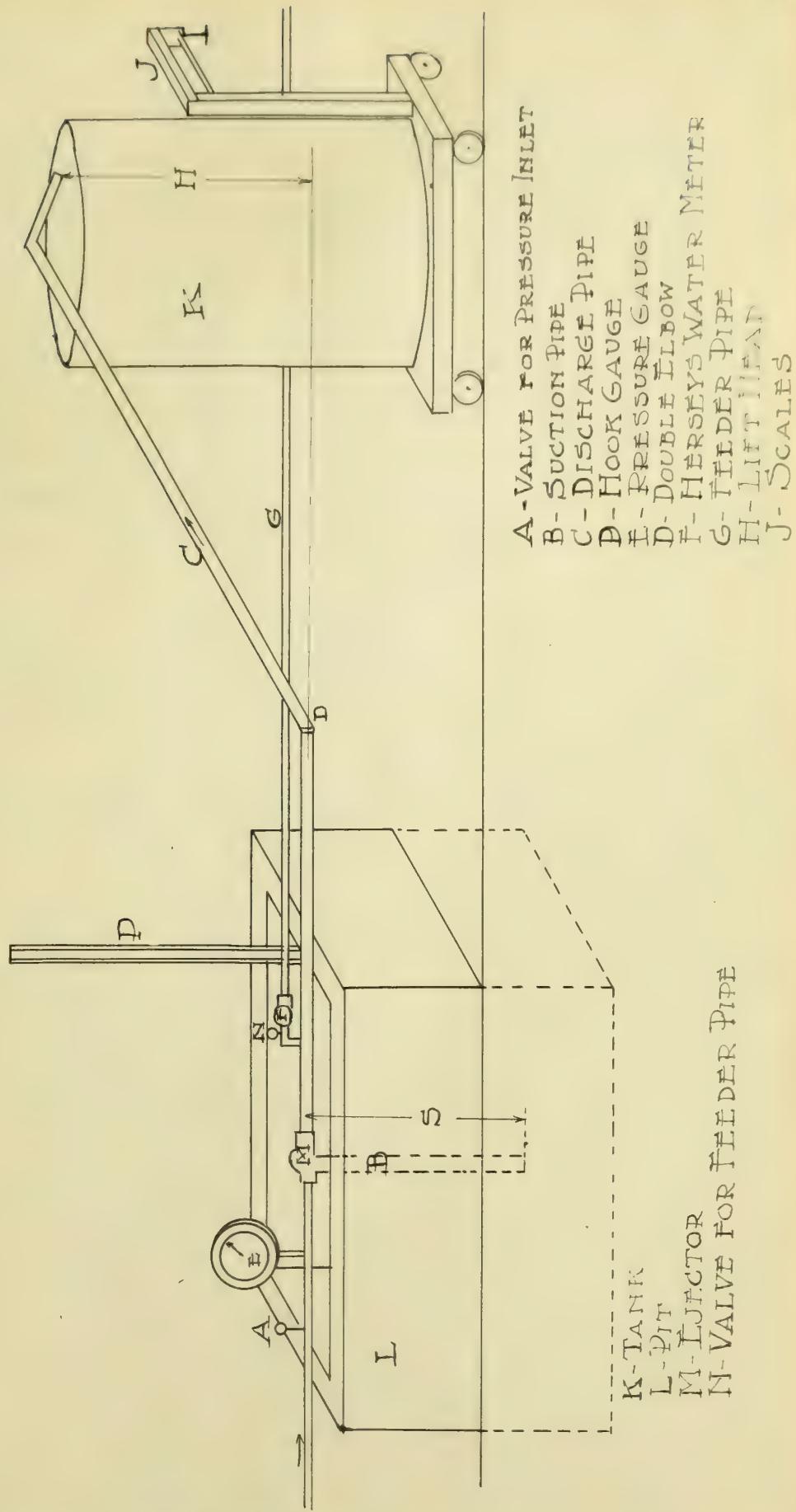
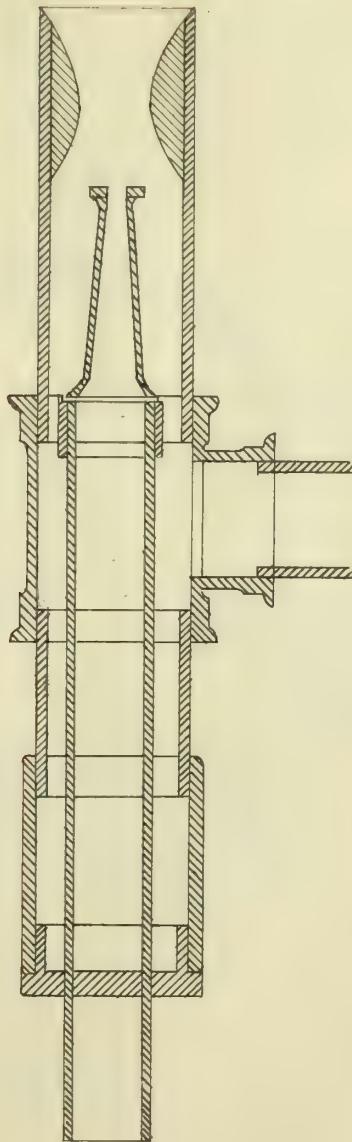
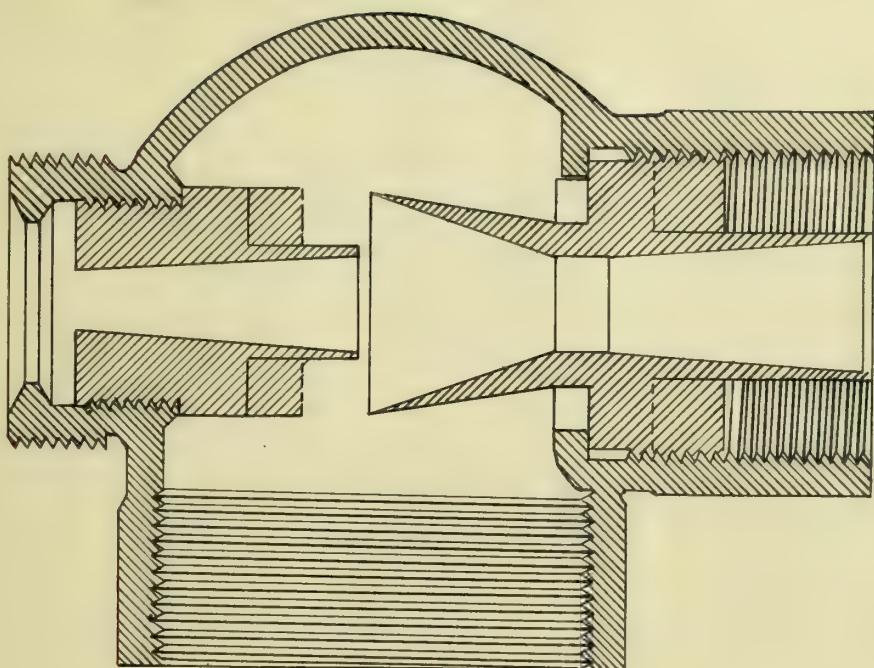


PLATE 2.

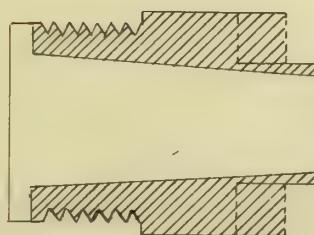


JET PUMP

PLATE 3



CHICAGO EJECTOR



MODIFIED NIPPLE

TABLE A.

TEST OF A ONE INCH CHICAGO EJECTOR.

No	PRESSURE HEAD IN FEET	SUCTION HEAD IN FEET	TOTAL HEAD IN FEET	WATER PUMPED IN CUBIC FEET	WATER USED IN CUBIC FEET	EFFICIENCY IN PER CENT	GAL. PUMPED PER GAL. USED
1	90	5.0	6.8	0.0317	0.0407	7.90	0.778
2	70	5.0	6.8	0.0226	0.0351	8.83	0.645
3	50	5.0	6.8	0.0081	0.0336	6.88	0.231
4	90	5.0	7.8	0.0271	0.0429	8.30	0.632
5	70	5.0	7.8	0.0179	0.0371	9.46	0.482
6	50	5.0	7.8	0.0050	0.0340	7.90	0.147
7	90	5.0	8.8	0.0276	0.0413	10.76	0.669
8	70	5.0	8.8	0.0185	0.0366	11.79	0.550
9	50	5.0	8.8	0.0016	0.0348	8.42	0.046
10	90	3.0	6.8	0.0254	0.0507	8.04	0.502
11	70	3.0	6.8	0.0194	0.0363	10.62	0.577
12	50	3.0	6.8	0.0080	0.0313	11.10	0.255
13	80	3.0	5.8	0.0264	0.0396	8.42	0.668
14	70	3.0	5.8	0.0219	0.0371	8.84	0.590
15	50	3.0	5.8	0.0103	0.0325	9.35	0.262
16	80	3.0	5.1	0.0264	0.0417	6.63	0.633
17	60	3.0	5.1	0.0262	0.0360	7.52	0.728
18	40	3.0	5.1	0.0170	0.0258	7.53	0.660
19	60	0.3	2.3	0.0226	0.0364	5.68	0.621

TABLE A, CONTINUED

TEST OF A ONE INCH CHICAGO EJECTOR

No	PRESSURE IN FEET	SUCTION HEAD IN FEET	TOTAL HEAD IN FEET	WATER PUMPED IN CUBIC FEET	EFFICIENCY IN PER CENT	GAL. PUMPED PER GAL. USED	
						WATER USED IN CUBIC FEET	PER CENT
20	40	0.3	2.3	0.0129	0.0309	7.40	0.417
21	30	0.3	2.3	0.0072	0.0291	8.58	0.248
22	60	0.3	3.3	0.0201	0.0350	8.17	0.575
23	45	0.3	3.3	0.0112	0.0322	9.22	0.348
24	30	0.3	3.3	0.0032	0.0295	11.20	0.108
25	70	0.3	4.3	0.0240	0.0365	9.77	0.657
26	50	0.3	4.3	0.0104	0.0342	9.70	0.304
27	60	4.9	11.0	0.0027	0.0355	10.70	0.076
28	60	4.9	9.6	0.0061	0.0416	10.18	0.146
29	50	0.4	6.6	0.0058	0.0378	14.40	0.153
30	55	0.4	5.1	0.0121	0.0439	11.10	0.276

TABLE B.

TEST OF A MODIFIED CHICAGO EJECTOR

No	PRESSURE HEAD IN FEET	SUCTION HEAD IN FEET	TOTAL HEAD IN FEET	WATER PUMPED IN CUBIC FEET	WATER USED IN CUBIC FEET	EFFICIENCY IN PER CENT	GAL. PUMPED PER GAL. USED
1	60	3.0	6.8	0.0385	0.0575	13.9	0.670
2	50	3.0	6.8	0.0327	0.0538	15.4	0.608
3	40	3.0	6.8	0.0248	0.0492	18.1	0.504
4	30	3.0	6.8	0.0224	0.0384	26.6	0.584
5	50	3.0	5.8	0.0341	0.0528	13.0	0.645
6	35	3.0	5.8	0.0254	0.0441	17.5	0.575
7	20	3.0	5.8	0.0136	0.0341	27.9	0.399
8	50	3.0	4.8	0.0349	0.0535	10.0	0.652
9	35	3.0	4.8	0.0278	0.0436	12.8	0.638
10	20	3.0	4.8	0.0210	0.0300	25.8	0.700
11	60	0.5	2.3	0.0490	0.0515	6.9	0.952
12	40	0.5	2.3	0.0358	0.0416	9.9	0.860
13	20	0.5	2.3	0.0193	0.0337	15.6	0.573
14	60	0.5	3.3	0.0428	0.0546	9.0	0.785
15	40	0.5	3.3	0.0316	0.0456	12.7	0.693
16	20	0.5	3.3	0.0175	0.0337	20.2	0.520
17	40	0.5	4.3	0.0271	0.0394	17.9	0.688
18	20	0.5	4.3	0.0149	0.0332	28.6	0.449

TABLE C.

TEST OF JET PUMP MADE OF PIPE FITTINGS.

No.	PRESSURE HEAD IN FEET	SUCTION HEAD IN FEET	TOTAL HEAD IN FEET	WATER PUMPED IN CUBIC FEET	WATER USED IN CUBIC FEET	EFFICIENCY IN PER CENT	GAL. PUMPED PER GAL. USED
1	6.0	2.00	5.29	0.0156	0.0360	9.30	0.434
2	4.6	2.00	5.29	0.0058	0.0234	10.78	0.214
3	4.5	4.00	5.80	0.0067	0.0424	6.03	0.158
4	3.5	1.80	3.40	0.0058	0.0297	5.50	0.195
5	3.5	1.80	3.40	0.0066	0.0285	6.70	0.221

TABLE D.

CHICAGO EJECTOR

PRESSURE HEAD	GAL PUMPED PER GAL USED						
	TOTAL HEAD		TOTAL HEAD		TOTAL HEAD		
	LIFT	SUCTION	LIFT	SUCTION	LIFT	SUCTION	
	1.8	5.0	2.8	5.0	3.8	5.0	
90	0.778		0.632		0.669		
70	0.645		0.482		0.550		
50	0.231		0.147		0.046		
TOTAL HEAD		TOTAL HEAD		TOTAL HEAD			
LIFT	SUCTION	LIFT	SUCTION	LIFT	SUCTION		
	3.8	3.0	2.8	3.0	2.1	3.0	
90	0.502						
80			0.668		0.633		
70	0.577		0.590				
60					0.728		
50	0.255		0.262				
40					0.660		
TOTAL HEAD		TOTAL HEAD		TOTAL HEAD			
LIFT	SUCTION	LIFT	SUCTION	LIFT	SUCTION		
	2.0	0.3	3.0	0.3	4.0	0.3	
70					0.657		
60	0.625		0.575				
50					0.304		
45			0.348				
40	0.417						
30	0.248		0.108				
TOTAL HEAD		TOTAL HEAD		TOTAL HEAD			
LIFT	SUCTION	LIFT	SUCTION	LIFT	SUCTION		
	6.1	4.9	4.7	4.9			
60	0.076		0.146				
TOTAL HEAD		TOTAL HEAD		TOTAL HEAD			
LIFT	SUCTION						
	6.6	0.4					
50	0.153						

TABLE E

MODIFIED CHICAGO EJECTOR

PRESSURE HEAD	GAL. PUMPED PER GAL. USED					
	TOTAL HEAD		TOTAL HEAD		TOTAL HEAD	
	LIFT	SUCTION	LIFT	SUCTION	LIFT	SUCTION
	3.8	3.0	2.8	3.0	1.8	3.0
60	0.670					
50	0.608		0.645		0.652	
40	0.504					
35			0.575		0.638	
30	0.584					
20			0.399		0.700	
TOTAL HEAD			TOTAL HEAD		TOTAL HEAD	
LIFT	SUCTION		LIFT	SUCTION	LIFT	SUCTION
	1.8	0.5	2.8	0.5	3.8	0.5
60	0.952		0.785			
40	0.860		0.693		0.688	
20	0.573		0.520		0.449	

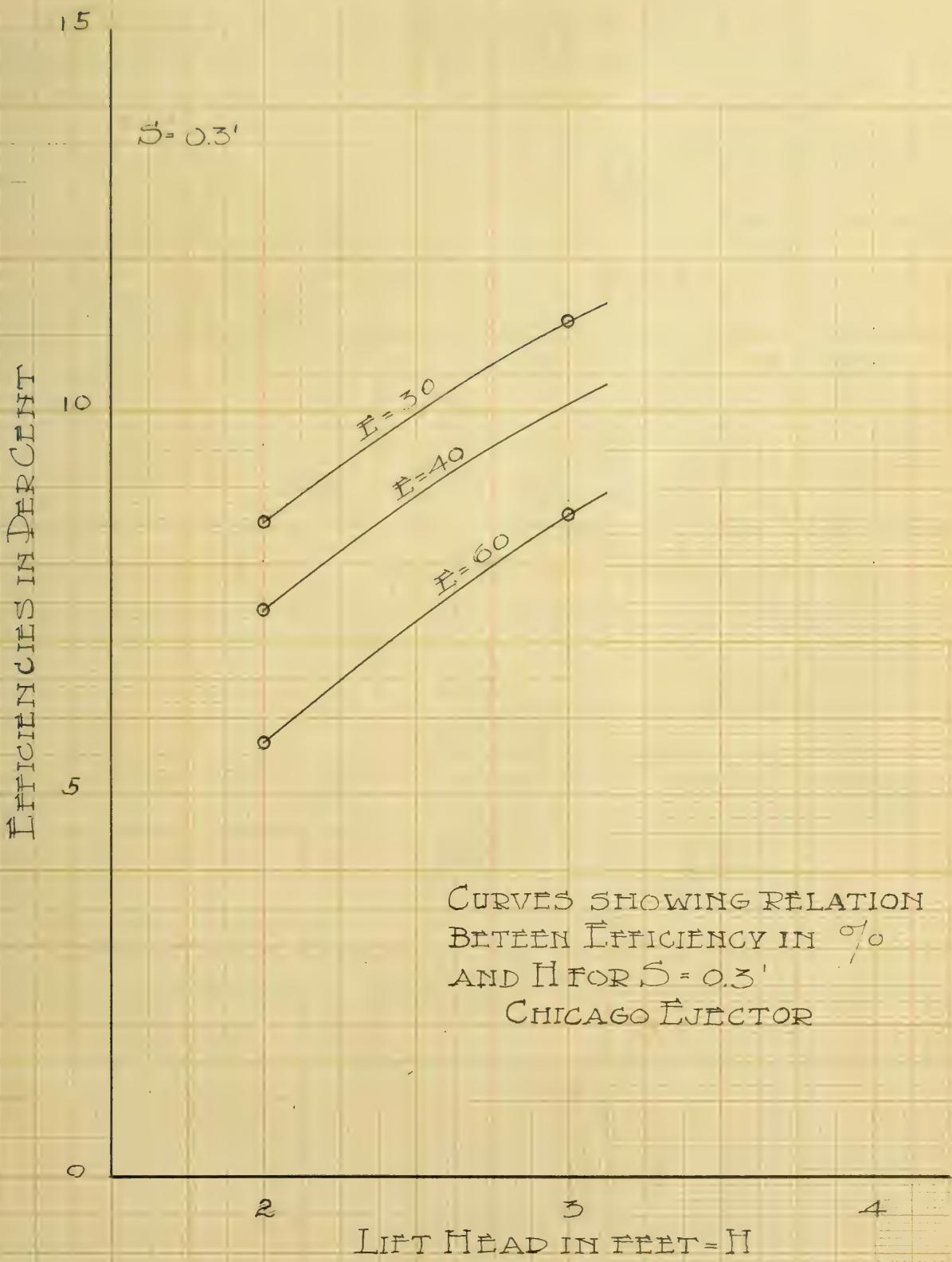
TABLE F

CALIBRATION OF A HERSEY'S METER

INITIAL WEIGHT W ₁	FINAL WEIGHT W ₂	W ₂ - W ₁ IN POUNDS	INITIAL METER R ₁	FINAL METER R ₂	R ₂ - R ₁ IN CUBIC FEET	W ₂ - W ₁ IN CUBIC FEET
913	1129	316	1219.50	1224.70	5.20	5.06
1229	1512	283	1229.25	4.55	4.53	
1512	1828	316	1234.40	5.15	5.06	
485	765	280	1239.02	4.62	4.48	
765	1105	340	1244.10	5.58	5.44	
1105	1422	317	1249.80	5.20	5.07	
1422	1739	317	1255.00	5.20	5.07	
470	1016	546	1264.00	9.00	8.74	
937	1553	616	1284.00	10.00	9.87	
446	1612	1166	1274.00	1303.00	19.00	18.55
TOTAL			73.50	71.81		

$$\frac{71.81}{73.50} = .978 \text{ CALIBRATION CONSTANT}$$

CURVE SHEET 1



CURVE SHEET 2.

EFFICIENCIES IN PER CENT

 $S = 3.0'$

10

5

0



CURVES SHOWING RELATION
BETWEEN EFFICIENCY IN %
AND H FOR $S = 3.0'$

CHICAGO EJECTOR

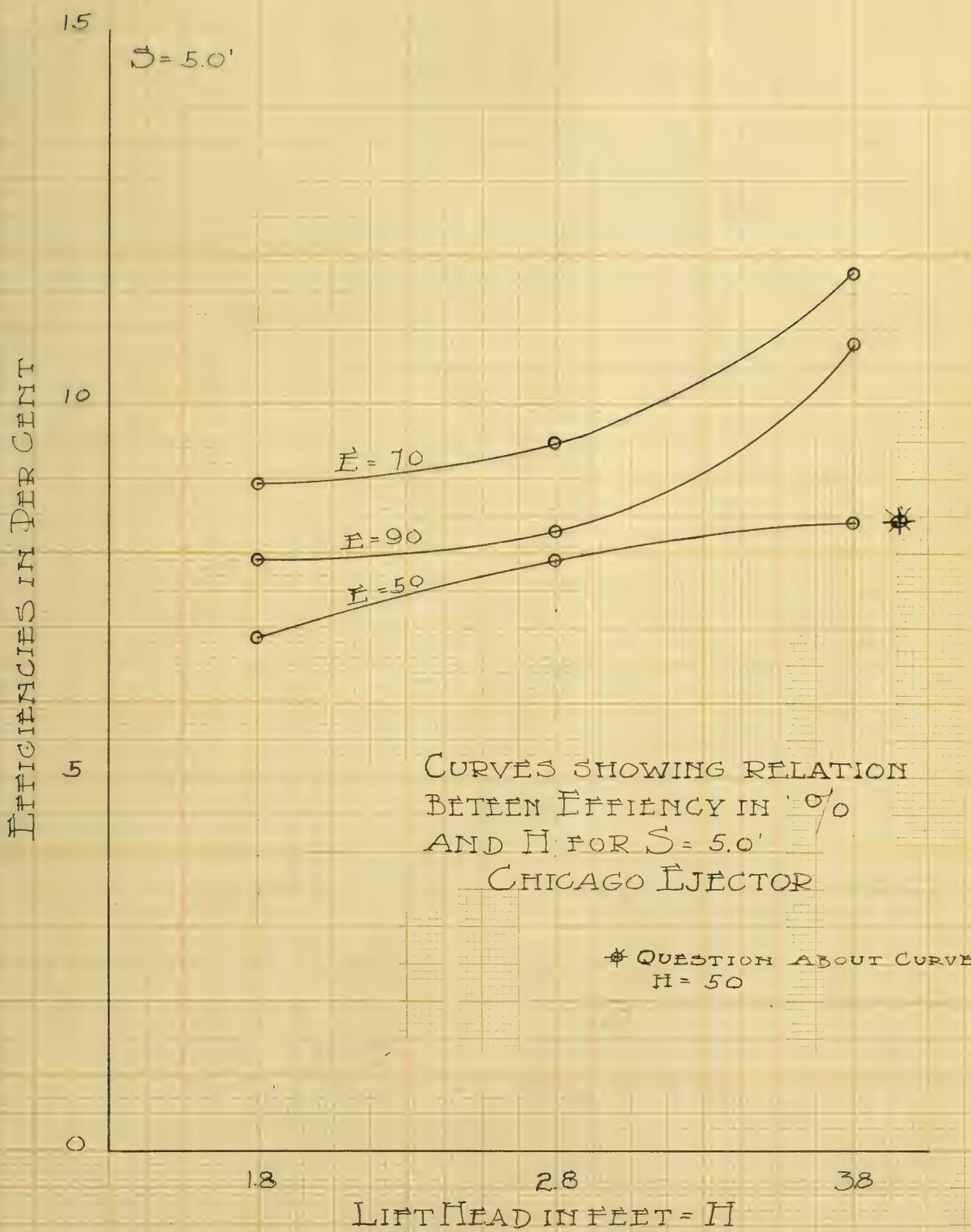
1.8

2.8

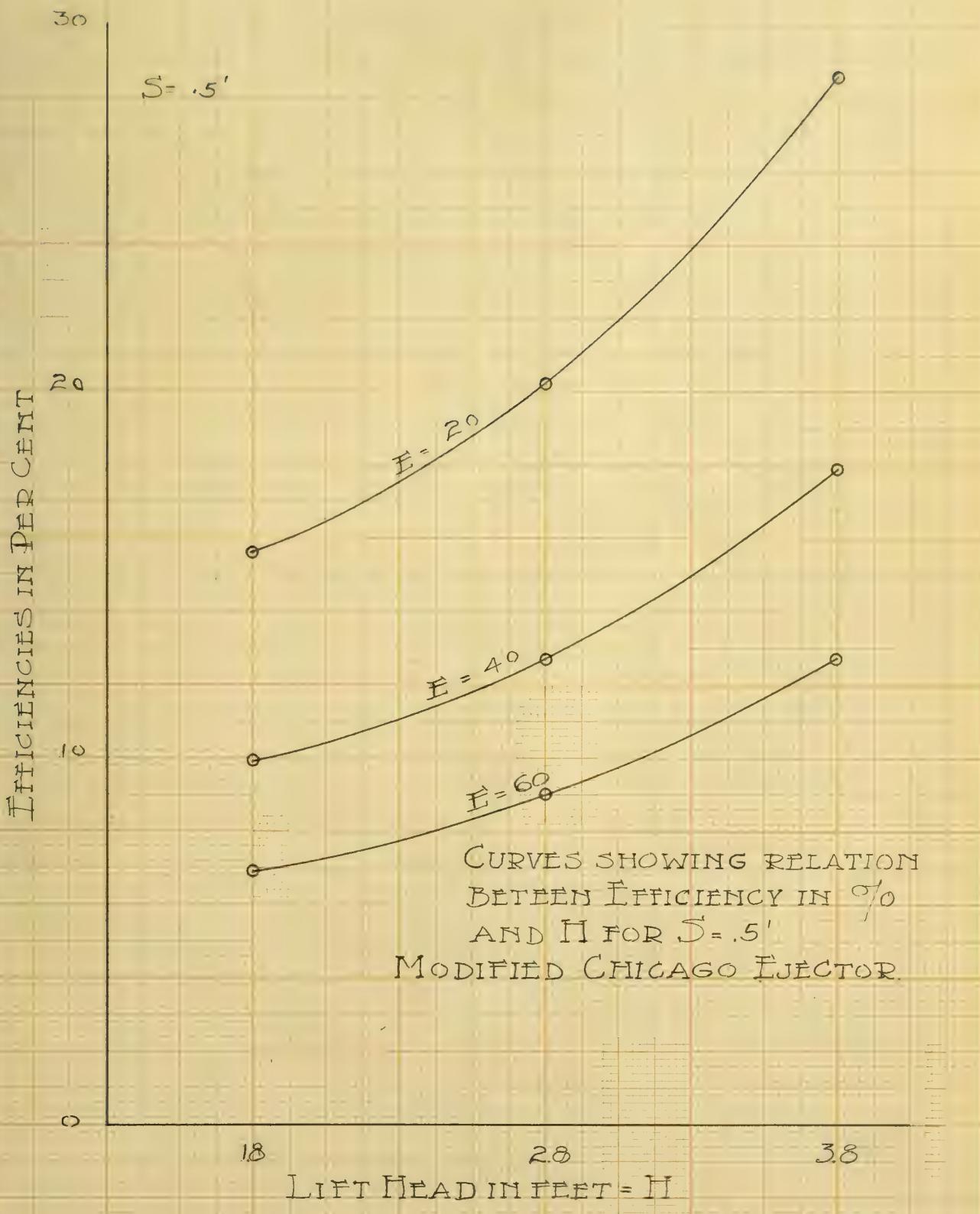
3.8

LIFT HEAD IN FEET = H

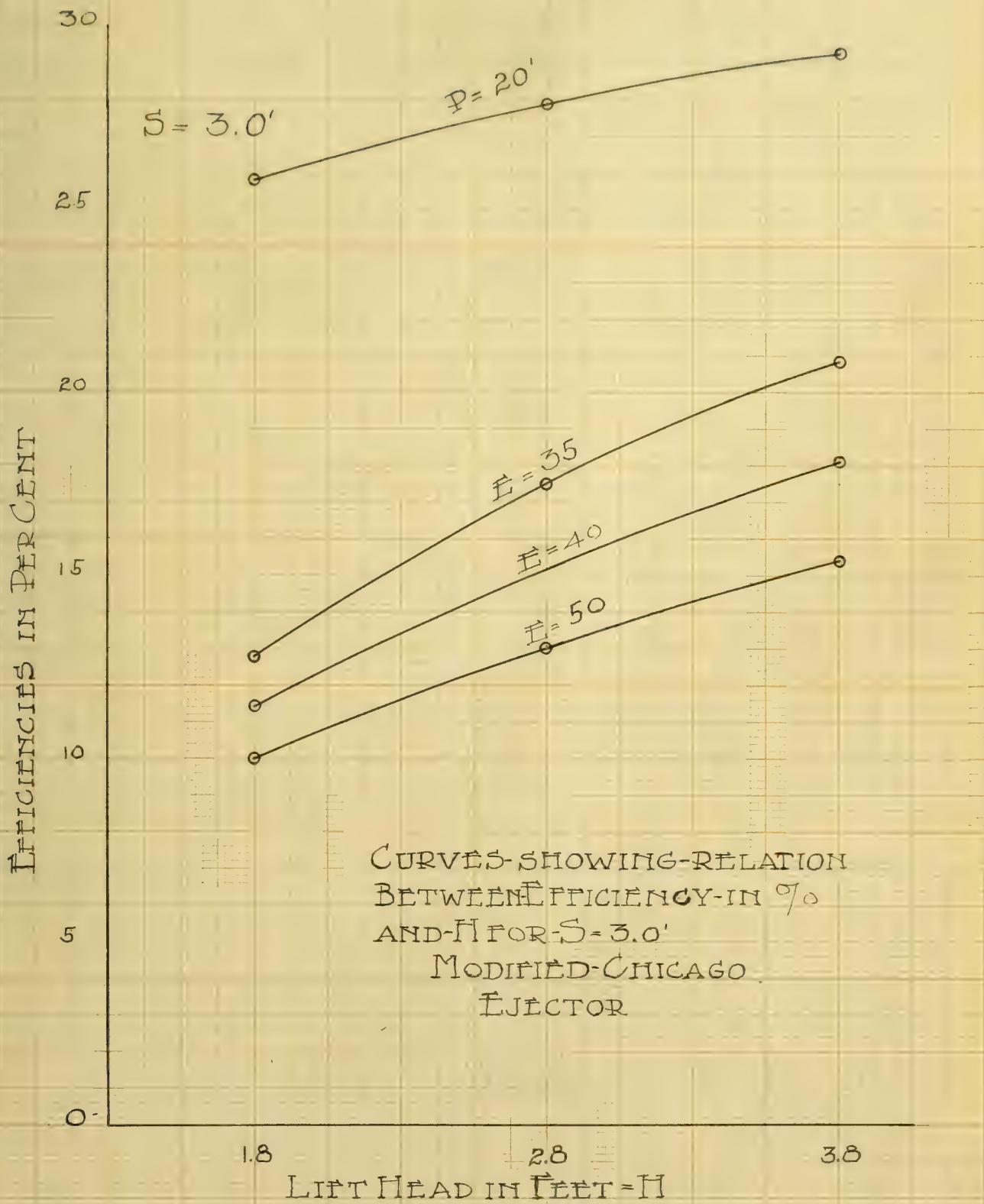
CURVE SHEET 3



CURVE SHEET 1



CURVE SHEET 5.



Conclusions

A few preliminary experiments the results of which are shown in table C were made with the jet pump which was built up of pipe fittings. These experiments were made more to find out whether this style of pump would work than to make a thorough investigation of its efficiencies. The results show that the efficiencies are lower than those obtained with the Chicago Ejector. This is due, at least partially to the fact that in the ejector used some little trouble was experienced in keeping the jet from impinging against the inside walls of the discharge tube, thereby causing impact losses. There was also some difficulty found in keeping the joints air-tight. Although the results of table C do not compare favorably with those of tables A and B, yet they do show that an ejector built up in this way will

give fairly good results.

The results of the experiments performed with the two forms of the Chicago Ejector are shown in tables A and B. The columns under the head of 'Efficiency' show the ratio of the work done to the energy expended. The column headed 'Gallons pumped per gallon used' shows the quantity of water pumped per gallon used. The best method of explaining the tables is to study the curve sheets 1 to 5.

The ordinates of these curves represent the efficiency in per cent. The abscissas represent the lift heads in feet and for these two variables the pressure head P and the suction head S remain constant for each curve. Curve sheets 1, 2 and 3 are obtained from the experiments found in table A. It will be found in studying these curves that the efficiencies do not in any case range higher

27

than 12%. The high heat efficiency obtained not plotted in curve sheets was 14.4 shown in experiment 29. This result was obtained by using a low suction head with a high lift head. The curves shown on sheet 3 for pressure heads of 70 and 90 feet curve in the opposite direction from the one shown for 50 feet and also from those shown on sheets 1 and 2. The facts shown most plainly from the curves on these sheets are:

- (1) The efficiency is affected to a considerable extent by the lift head. The greater the value of H , the higher the efficiency.
- (2) The efficiency is affected by the pressure head H and also by the suction head S . The best combination of these two quantities for high efficiency is to use a low suction head with a low pressure head or a high suction head with a high pressure head.

Curve sheets 4 and 5, which were plotted from table B show that the efficiencies obtained by using the modified ejector, range quite a little higher than those obtained by using the original ejector. The facts given above can be applied here with the exception that although the efficiency is affected by the suction head and pressure head, yet the low pressure head gives the best efficiency with a low and also a medium high suction head. Tables D and E show the number of gallons pumped per gallon used for different values of I, II and S. These tables could not be filled out completely as there were not enough experiments made to do so.

In general, the number of gallons pumped per gallon used is decreased:

- (1) As the lift head increases
- (2) As the suction head increases

(3) As the pressure head decreases in general we find that this quantity decreases as the efficiency increases.

The advantages of this style of pump are:

(1) It has no valves or parts that wear out easily

(2) It can pump muddy water.

(3) It is very suitable for sewer work where high efficiency is not required.

(4) It is simple, light and easy to operate, easy to set up and easy to move.

The main disadvantage is that it is not an efficient pump.





UNIVERSITY OF ILLINOIS-URBANA



3 0112 086764435